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FORM (REV I	PTO-139 1-98)	90 (Modified) U.S. DEPARTMENT	OF COMMERCE PATENT AND TRADEMARK OFFICE	ATTORNEY'S DOCKET NUMBER	
			TO THE UNITED STATES	JMYT-217US	
		DESIGNATED/ELECTI	U.S. APPLICATION NO. (IF KNOWN, SEE 37 CFR 1.5)		
		CONCERNING A FILIN	To be Oslandi 601694		
INTE		TONAL APPLICATION NO.  PCT/GB99/00292	PRIORITY DATE CLAIMED  6 February 1998 (06.02.98)		
TITL	E OF I	NVENTION			
IMP	ROV	EMENTS IN CATALYTIC	REDUCTION OF NOx		
APPL	ICAN'	T(S) FOR DO/EO/US			
And	ers A	ANDREASSON, Guy Richard	CHANDLER, Claus Friedrich GOER	SMANN, and James Patrick WARREN	
Appl	icant l	herewith submits to the United St	ates Designated/Elected Office (DO/EO/US)	the following items and other information:	
1.	X	This is a FIRST submission of i	items concerning a filing under 35 U.S.C. 371	l.	
2.		This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371.			
3.	×	This is an express request to be examination until the expiration	gin national examination procedures (35 U.S.) of the applicable time limit set in 35 U.S.C.	C. 371(f)) at any time rather than delay 371(b) and PCT Articles 22 and 39(1).	
4.	X			e 19th month from the earliest claimed priority date.	
5.	$\boxtimes$	A copy of the International Appl	ication as filed (35 U.S.C. 371 (c) (2))		
İ		a.   is transmitted herewith (required only if not transmitted by the International Bureau).			
		b.   has been transmitted by	y the International Bureau.		
1		c. $\square$ is not required, as the a	application was filed in the United States Rec	eiving Office (RO/US).	
6.		A translation of the International Application into English (35 U.S.C. 371(c)(2)).			
7.	$\boxtimes$	A copy of the International Search Report (PCT/ISA/210).			
8.	$\boxtimes$	Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371 (c)(3))			
			th (required only if not transmitted by the Inte by the International Bureau.	ernational Bureau).	
			owever, the time limit for making such amend	lments has NOT expired	
1		d. \( \) have not been made an	_		
9.		A translation of the amendments	to the claims under PCT Article 19 (35 U.S.	C. 371(c)(3)).	
10.	×	An oath or declaration of the inv	·		
11.	$\boxtimes$	A copy of the International Preli	minary Examination Report (PCT/IPEA/409).		
12.		A translation of the annexes to to (35 U.S.C. 371 (c)(5)).	A translation of the annexes to the International Preliminary Examination Report under PCT Article 36		
I	tems :	13 to 20 below concern documen	it(s) or information included:		
13.		An Information Disclosure State	ement under 37 CFR 1.97 and 1.98.	V.	
14.		An assignment document for rec	ording. A separate cover sheet in compliance	with 37 CFR 3.28 and 3.31 is included.	
15.	$\boxtimes$	A FIRST preliminary amendme	nt.		
16.		A SECOND or SUBSEQUENT	preliminary amendment.		
17.		A substitute specification.			
18.		A change of power of attorney as	nd/or address letter.		
19.	$\boxtimes$	Certificate of Mailing by Expres	s Mail		
20.		Other items or information:			
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						DOCKET NUMBER
This assissed 1674	APPLICATION NO. (15 KNOWN SEE 37 CFR 1.5)  10 by assigned 1 0 4 INTERNATIONAL APPLICATION NO.  PCT/GB99/00292				JMY	Γ-217US
21. The following fees are submitted:.					CALCULATIONS	S PTO USE ONLY
BASIC NATIONAL FEE ( 37 CFR 1.492 (a) (1) -	· (5)) :					
international search fee (37 CFR 1 445(a)(2))	- C (07 CTD 1 400)					
International preliminary examination fee (37 CFR 1.482) not paid to USPTO but Internation Search Report prepared by the EPO or JPO				.00		
☐ International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO				.00		
☐ International preliminary examination fee paid to USPTO (37 CFR 1.482) but all claims did not satisfy provisions of PCT Article 33(1)-(4)			.00			
<ul> <li>International preliminary examination fee pa and all claims satisfied provisions of PCT Ar</li> </ul>	id to USPTO (37 CFR 1.482) ticle 33(1)-(4)		\$96	5.00		
	ATE BASIC FEE AN	10t	INT =		\$840.00	
Surcharge of \$130.00 for furnishing the oath or decl months from the earliest claimed priority date (37.0	aration later than CFR 1.492 (e)).	20	□ 30		\$0.00	
CLAIMS NUMBER FILED	NUMBER EXTRA		RATE			
Total claims 12 - 20 =	0	x	\$18.00		\$0.00	
Independent claims 3 - 3 =	0	X	\$78.00		\$0.00 \$0.00	
Multiple Dependent Claims (check if applicable).	ABOVE CALCULA	TIO	NIC		\$840.00	
Reduction of 1/2 for filing by small entity, if applic must also be filed (Note 37 CFR 1.9, 1.27, 1.28) (c	able. Verified Small Entity S				\$0.00	
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Processing fee of \$130.00 for furnishing the English months from the earliest claimed priority date (37.0)	CFR 1.492 (f)).			+	\$0.00	
	TOTAL NATIONA	LF	EE	=	\$840.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31) (check if applicable).  TOTAL FEES ENCLOSED = \$840.00						
Ar				Amount to be: refunded	\$	
charged \$					\$	
A check in the amount of \$840.00  Please charge my Deposit Account No. A duplicate copy of this sheet is enclosed.	to cover the above fees is of in the amount		ed.		to cover the abo	ve fees.
The Commissioner is hereby authorized to charge any fees which may be required, or credit any overpayment to Deposit Account No. 18-0350 A duplicate copy of this sheet is enclosed.						
NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.						
SEND ALL CORRESPONDENCE TO:						
Paul F. Prestia SIGNATURE						
Ratner & Prestia Suite 301, One Westlakes (Berwyn) Christopher R. Lewis						
P.O. Box 980						
Valley Forge, PA 19482  NAME						
Phone: (610) 407-0700						
Fax: (610) 407-0701		F	ÆGISTF	OITAS	ON NUMBER	
		A	August '	7, 200	00	
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**PATENT** 

## IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant:

Anders Andreasson et al.

: Art Unit:

Application No.:

09/601,694

: Examiner:

Filed:

August 7, 2000

FOR: IMPROVEMENTS IN CATALYTIC

REDUCTION OF NOx

# SUPPLEMENTAL PRELIMINARY AMENDMENT

**Assistant Commissioner for Patents** Washington, DC 20231

SIR:

as follows.

Prior to examination, please amend the above-identified application

## IN THE SPECIFICATION:

On page 1, after the title, please insert the following sentence:

-- This application is the U.S. national phase application of International Application No. PCT/GB99/00292.--

Respectfully submitted,

Christopher R. Lewis, Reg. No. 36,201

Attorney for Applicants

CRL/lrb

Dated: January 9, 2001

Suite 301

One Westlakes, Berwyn

P.O. Box 980

Valley Forge, PA 19482-0980

(610) 407-0700

The Assistant Commissioner for Patents is hereby authorized to charge payment to Deposit Account No. 18-0350 of any fees associated with this communication.

EXPRESS MAIL Mailing Label No.: EL736965403US

Date of Deposit: January 9, 2001

I hereby certify that this paper and fee are being deposited, under 37 C.F.R. § 1.10 and with sufficient postage, using the "Express Mail Post Office to Addressee" service of the United States Postal Service on the date indicated above and that the deposit is addressed to the Assistant Commissioner for Patents, Washington, D.C. 20231.

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# IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant: Anders Andreasson et al. : Art Unit:
Serial No.: To be Assigned : Examiner:

Filed: : Herewith :

FOR: : IMPROVEMENTS IN CATALYTIC :

REDUCTION OF NOx :

#### PRELIMINARY AMENDMENT

Assistant Commissioner for Patents Washington, D.C. 20231
Box PCT

SIR:

Prior to examination, please amend the above-identified application as follows.

#### IN THE CLAIMS:

Please amend the following claims:

1. (Amended) An improved SCR system for treating combustion exhaust gas containing [NO] NO<sub>x</sub> and particulates, comprising [in combination and in or,] an oxidation catalyst effective to convert at least a portion of NO in said NO<sub>x</sub> to NO<sub>2</sub> thereby enhancing [and enchance] the NO<sub>2</sub> content of the exhaust gas, a particulate trap, a source of reductant fluid, [injections] injection means for [such] said reductant fluid located downstream of said particulate trap and an SCR catalyst.

3. (Amended) An SCR system according to claim 1 [or 2], wherein the oxidation catalyst is a platinum catalyst carried on a through-flow honeycomb support.

4. (Amended) An SCR system according to [claims 1,2 or 3] <u>claim</u>
2 <u>1,</u> wherein the particulate filter is a wall-flow filter.

5. (Amended) An SCR system according to [any one of the preceding claims] <u>claim 1</u>, <u>further</u> comprising [also] means to cool gases upstream of the SCR catalyst.

- 6. (Amended) An SCR system according to claim 5, <u>further</u> comprising [also] control means such that said gas cooling means is activated only when a high SCR catalyst temperature is detected or conditions are determined that are expected to lead to high catalyst temperatures.
- 7. (Amended) A diesel engine provided with an SCR system [according to any one of claims 1 to 5] for treating combustion exhaust gas containing NO<sub>x</sub> and particulates, said SCR system comprising an oxidation catalyst effective to convert at least a portion of NO in said NO<sub>x</sub> to NO<sub>2</sub> thereby enhancing the NO<sub>2</sub> content of the exhaust gas, a particulate trap, a source of reductant fluid, injection means for said reductant fluid located downstream of said particulate trap and an SCR catalyst.
- 8. (Amended) A [light duty] diesel engine according to claim [6] 7, wherein the volume of the exhaust gas after-treatment system is reduced and the diesel engine is light duty.
- 9. (Amended) A method of reducing pollutants, including particulates and NO<sub>x</sub>, in <u>a</u> gas [streams] <u>stream</u>, comprising passing [such] <u>said</u> gas stream over an oxidation catalyst under conditions effective to convert at least a portion of NO in the gas stream to NO<sub>2</sub> [and enhance] <u>thereby enhancing</u> the NO<sub>2</sub> content of the gas stream, removing at least a portion of said particulates in a particulate trap, reacting trapped particulate with NO<sub>2</sub>, adding reductant fluid to the gas stream to form a gas mixture downstream of said trap, and passing the gas mixture over an SCR catalyst under NO<sub>x</sub> reduction conditions.
- 11. (Amended) A method according to claims 9 [or 10], wherein the [gases are] gas stream or gas mixture is cooled[, if necessary,] before reaching the SCR catalyst.

1 12. (Amended) A method according to claim 9[, 10 or 11], wherein the NO to NO<sub>2</sub> ratio of the [gases] gas mixture is adjusted to a level pre-determined to be optimum for the SCR catalyst, by oxidation of NO over [an] said oxidation catalyst.

### REMARKS

The Assistant Commissioner is hereby authorized to charge payment to Deposit Account No. 18-0350 of any fees associated with this communication.

Respectfully submitted,

Paul F. Prestia, Reg. No. 23,031

Christopher R. Lewis, Reg. No. 36,201

Attorney for Applicants

/bgd

Dated: August 7, 2000

Suite 301 1 Westlakes, Berwyn P.O. Box 980 Valley Forge, PA 19482 (610) 407-0700

**EXPRESS MAIL Mailing Label Number: Date of Deposit:** 

EL541609846US August 7, 2000

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Kathleen Libby

The present invention concerns improvements in selective catalytic reduction of NOx in waste gas streams such as diesel engine exhausts or other lean exhaust gases such as from gasoline direct injection (GDI).

EP 0 758 713 (Toyota) describes a method for purifying the exhaust gas of a diesel engine which uses a catalyst to convert NO in the exhaust gas to NO<sub>2</sub>, thereafter trapping particulate in a filter and oxidising the particulate by reaction with the NO<sub>2</sub>. The exhaust gas is thereafter fed to a NO<sub>x</sub> absorbent or, in one embodiment, to a NO<sub>x</sub> conversion catalyst. Unburnt hydrocarbons and CO in the exhaust gas are trapped in a zeolite and released to react with NO<sub>x</sub> on the NO<sub>x</sub> conversion catalyst.

The technique named SCR (Selective Catalytic Reduction) is well established for industrial plant combustion gases, and may be broadly described as passing a hot exhaust gas over a catalyst in the presence of a nitrogenous reductant, especially ammonia or urea. This is effective to reduce the NOx content of the exhaust gases by about 20-25% at about 250 °C, or possibly rather higher using a platinum catalyst, although platinum catalysts tend to oxidise NH<sub>3</sub> to NOx during higher temperature operation. We believe that SCR systems have been proposed for NOx reduction for vehicle engine exhausts, especially large or heavy duty diesel engines, but this does require on-board storage of such reductants, and is not believed to have met with commercial acceptability at this time.

We believe that if there could be a significant improvement in performance of SCR systems, they would find wider usage and may be introduced into vehicular applications. It is an aim of the present invention to improve significantly the conversion of NOx in a SCR system, and to improve the control of other pollutants using a SCR system.

Accordingly, the present invention provides an improved SCR catalyst system for treating combustion exhaust gas containing NO and particulates, comprising in combination and in order, an oxidation catalyst effective to convert NO to NO<sub>2</sub> and enhance the NO<sub>2</sub>

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content of the exhaust gas, a particulate filter, a source of reductant fluid, injection means for said reductant fluid located downstream of said particulate trap and an SCR catalyst.

The invention further provides an improved method of reducing pollutants, including particulates and NOx in gas streams, comprising passing such gas stream over an oxidation catalyst under conditions effective to convert at least a portion of NO in the gas stream to NO<sub>2</sub>, and enchance the NO<sub>2</sub> content of the gas stream, removing at least a portion of said particulates in a particulate trap, reacting trapped particulate with NO<sub>2</sub>, adding reductant fluid to the gas stream to form a gas mixture downstream of said trap, and passing the gas mixture over an SCR catalyst.

Although the present invention provides, at least in its preferred embodiments, the opportunity to reduce very significantly the NO<sub>x</sub> emissions from the lean (high in oxygen) exhaust gases from diesel and similar engines, it is to be noted that the invention also permits very good reductions in the levels of other regulated pollutants, especially hydrocarbons and particulates.

The invention is believed to have particular application to the exhausts from heavy duty diesel engines, especially vehicle engines, eg truck or bus engines, but is not to be regarded as being limited thereto. Other applications might be LDD (light duty diesel), GDI, CNG (compressed natural gas) engines, ships or stationary sources. For simplicity, however, the majority of this description concerns such vehicle engines.

We have surprisingly found that a "pre-oxidising" step, which is not generally considered necessary because of the low content of CO and unburnt fuel in diesel exhausts, is particularly effective in increasing the conversion of NOx to N<sub>2</sub> by the SCR system. We also believe that minimising the levels of hydrocarbons in the gases may assist in the conversion of NO to NO<sub>2</sub>. This may be achieved catalytically and/or by engine design or management. Desirably, the NO<sub>2</sub>/NO ratio is adjusted according to the present invention to the most beneficial such ratio for the particular SCR catalyst and CO and hydrocarbons are oxidized prior to the SCR catalyst. Thus, our preliminary results indicate that for a transition

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metal/zeolite SCR catalyst it is desirable to convert all NO to NO<sub>2</sub>, whereas for a rare earth-based SCR catalyst, a high ratio is desirable providing there is some NO, and for other transition metal-based catalysts gas mixtures are notably better than either substantially only NO or NO<sub>2</sub>. Even more surprisingly, the incorporation of a particulate filter permits still higher conversions of NOx.

The oxidation catalyst may be any suitable catalyst, and is generally available to those skilled in art. For example, a Pt catalyst deposited upon a ceramic or metal throughflow honeycomb support is particularly suitable. Suitable catalysts are e.g. Pt/Al2O3 catalysts, containing 1-150g Pt/ft<sup>3</sup> (0.035-5.3g Pt/litre) catalyst volume depending on the NO2/NO ratio required. Such catalysts may contain other components providing there is a beneficial effect or at least no significant adverse effect.

The source of reductant fluid conveniently uses existing technology to inject fluid into the gas stream. For example, in the tests for the present invention, a mass controller was used to control supply of compressed NH<sub>3</sub>, which was injected through an annular injector ring mounted in the exhaust pipe. The injector ring had a plurality of injection ports arranged around its periphery. A conventional diesel fuel injection system including pump and injector nozzle has been used to inject urea by the present applicants. A stream of compressed air was also injected around the nozzle; this provided good mixing and cooling.

The reductant fluid is suitably NH<sub>3</sub>, but other reductant fluids including urea, ammonium carbamate and hydrocarbons including diesel fuel may also be considered. Diesel fuel is, of course, carried on board a diesel-powered vehicle, but diesel fuel itself is a less selective reductant than NH<sub>3</sub> and is presently not preferred.

Suitable SCR catalysts are available in the art and include Cu-based and vanadia-based catalysts. A preferred catalyst at present is a V<sub>2</sub>O<sub>5</sub>/WO<sub>3</sub>/TiO<sub>2</sub> catalyst, supported on a honeycomb through-flow support. Although such a catalyst has shown good performance in the tests described hereafter and is commercially available, we have found that sustained high temperature operation can cause catalyst deactivation. Heavy duty diesel engines,

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which are almost exclusively turbocharged, can produce exhaust gases at greater than 500°C under conditions of high load and/or high speed, and such temperatures are sufficient to cause catalyst deactivation. In one embodiment of the invention, therefore, cooling means is provided upstream of the SCR catalyst. Cooling means may suitably be activated by sensing high catalyst temperatures or by other, less direct, means, such as determining conditions likely to lead to high catalyst temperatures. Suitable cooling means include water injection upstream of the SCR catalyst, or air injection, for example utilising the engine turbocharger to provide a stream of fresh intake air by-passing the engine. We have observed a loss of activity of the catalyst, however, using water injection, and air injection by modifying the turbocharger leads to higher space velocity over the catalyst which tends to reduce NOx conversion. Preferably, the preferred SCR catalyst is maintained at a temperature from 160°C to 450°C.

We believe that in its presently preferred embodiments, the present invention may depend upon an incomplete conversion of NO to NO<sub>2</sub>. Desirably, therefore, the oxidation catalyst, or the oxidation catalyst together with the particulate trap if used, yields a gas stream entering the SCR catalyst having a ratio of NO to NO<sub>2</sub> of from about 4:1 to about 1:3 by vol, for the commercial vanadia-type catalyst. As mentioned above, other SCR catalysts perform better with different NO/NO<sub>2</sub> ratios. We do not believe that it has previously been suggested to adjust the NO/NO<sub>2</sub> ratio in order to improve NOx reduction.

The present invention incorporates a particulate trap downstream of the oxidation catalyst. We discovered that soot-type particulates may be removed from a particulate trap by "combustion" at relatively low temperatures in the presence of NO<sub>2</sub>. In effect, the incorporation of such a particulate trap serves to clean the exhaust gas of particulates without causing accumulation, with resultant blockage or back-pressure problems, whilst simultaneously reducing a proportion of the NOx. Suitable particulate traps are generally available, and are desirably of the type known as wall-flow filters, generally manufactured from a ceramic, but other designs of particulate trap, including woven, knitted or non-woven heat-resistant fabrics, may be used.

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It may be desirable to incorporate a clean-up catalyst downstream of the SCR catalyst, to remove any NH<sub>3</sub> or derivatives thereof which could pass through unreacted or as by-products. Suitable clean-up catalysts are available to the skilled person.

A particularly interesting possibility arising from the present invention has especial application to light duty diesel engines (car and utility vehicles) and permits a significant reduction in volume and weight of the exhaust gas after-treatment system, in a suitable engineered system.

Several tests have been carried out in making the present invention. These are described below, and are supported by results shown in graphical form in the attached drawings.

A commercial 10 litre turbocharged heavy duty diesel engine on a test-bed was used for all the tests described herein.

### Test 1 - (Comparative)

A conventional SCR system using a commercial V<sub>2</sub>O<sub>5</sub>/WO<sub>3</sub>/TiO<sub>2</sub> catalyst, was adapted and fitted to the exhaust system of the engine. NH<sub>3</sub> was injected upstream of the SCR catalyst at varying ratios. The NH<sub>3</sub> was supplied from a cylinder of compressed gas and a conventional mass flow controller used to control the flow of NH<sub>3</sub> gas to an experimental injection ring. The injection ring was a 10cm diameter annular ring provided with 20 small injection ports arranged to inject gas in the direction of the exhaust gas flow. NOx conversions were determined by fitting a NOx analyser before and after the SCR catalyst and are plotted against exhaust gas temperature in Figure 1. Temperatures were altered by maintaining the engine speed constant and altering the torque applied.

A number of tests were run at different quantities of NH<sub>3</sub> injection, from 60% to 100% of theoretical, calculated at 1:1 NH<sub>3</sub>/NO and 4:3 NH<sub>3</sub>/NO2. It can readily be seen that at low temperatures, corresponding to light load, conversions are about 25%, and the highest

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conversions require stoichiometric (100%) addition of NH<sub>3</sub> at catalyst temperatures of from 325 to 400 °C, and reach about 90%. However, we have determined that at greater than about 70% of stoichiometric NH<sub>3</sub> injection, NH<sub>3</sub> slips through the SCR catalyst unreacted, and can cause further pollution problems.

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#### Test 2 (Comparative)

The test rig was modified by inserting into the exhaust pipe upstream of the NH<sub>3</sub> injection, a commercial platinum oxidation catalyst of 10.5 inch diameter and 6 inch length (26.67cm diameter and 15.24cm length) containing 10g Pt/ft<sup>3</sup> (= 0.35g/litre) of catalyst volume. Identical tests were run, and it was observed from the results plotted in Figure 2, that even at 225°C, the conversion of NOx has increased from 25% to >60%. The greatest conversions were in excess of 95%. No slippage of NH<sub>3</sub> was observed in this test nor in the following test.

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#### Test 3

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The test rig was modified further, by inserting a particulate trap before the NH<sub>3</sub> injection point, and the tests run again under the same conditions at 100% NH<sub>3</sub> injection and a space velocity in the range 40,000 to 70,000 hr<sup>-1</sup> over the SCR catalyst. The results are plotted and shown in Figure 3. Surprisingly, there is a dramatic improvement in NOx conversion, to above 90% at 225°C, and reaching 100% at 350°C. Additionally, of course, the particulates which are the most visible pollutant from diesel engines, are also controlled.

## 25 <u>Test 4</u>

An R49 test with 80% NH3 injection was carried out over a V2O5/WO3/TiO2 SCR catalyst. This gave 67% particulate, 89% HC and 87% NOx conversion; the results are plotted in Figure 4.

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Additionally tests have been carried out with a different diesel engine, and the excellent results illustrated in Test 3 and 4 above have been confirmed.

The results have been confirmed also for a non-vanadium SCR catalyst.

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#### **CLAIMS**

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- 1. An improved SCR system for treating combustion exhaust gas containing NO and particulates, comprising in combination and in order, an oxidation catalyst effective to convert and enchance the NO<sub>2</sub> content of the exhaust gas, a particulate trap, a source of reductant fluid, injections means for such reductant fluid located downstream of said particulate trap and an SCR catalyst.
- An SCR system according to claim 1, wherein the reductant fluid is NH<sub>3</sub>.
- 3. An SCR system according to claim 1 or 2, wherein the oxidation catalyst is a platinum catalyst carried on a through-flow honeycomb support.
- 4. An SCR system according to claims 1,2 or 3 wherein the particulate filter is a wall-flow filter.
- 5. An SCR system according to any one of the preceding claims, comprising also means to cool gases upstream of the SCR catalyst.
- 20 6. An SCR system according to claim 5, comprising also control means such that said gas cooling means is activated only when a high SCR catalyst temperature is detected or conditions are determined that are expected to lead to high catalyst temperatures.
  - 7. A diesel engine provided with an SCR system according to any one of claims 1 to 5.
  - 8. A light duty diesel engine according to claim 6, wherein the volume of the exhaust gas after-treatment system is reduced.
- A method of reducing pollutants, including particulates and NOx, in gas streams,
   comprising passing such gas stream over an oxidation catalyst under conditions effective to
   convert at least a portion of NO in the gas stream to NO<sub>2</sub> and enhance the NO<sub>2</sub> content of the



gas stream, removing at least a portion of said particulates in a particulate trap, reacting trapped particulate with  $NO_2$ , adding reductant fluid to the gas stream to form a gas mixture downstream of said trap, and passing the gas mixture over an SCR catalyst under NOx reduction conditions.

- 10. A method according to claim 9, wherein said gas stream is the exhaust from a diesel, GDI or CNG engine.
- 11. A method according to claim 9 or 10, wherein the gases are cooled, if necessary, before reaching the SCR catalyst.
- 12. A method according to claim 9, 10 or 11, wherein the NO to NO<sub>2</sub> ratio in the gases is adjusted to a level pre-determined to be optimum for the SCR catalyst, by oxidation of NO over an oxidation catalyst.

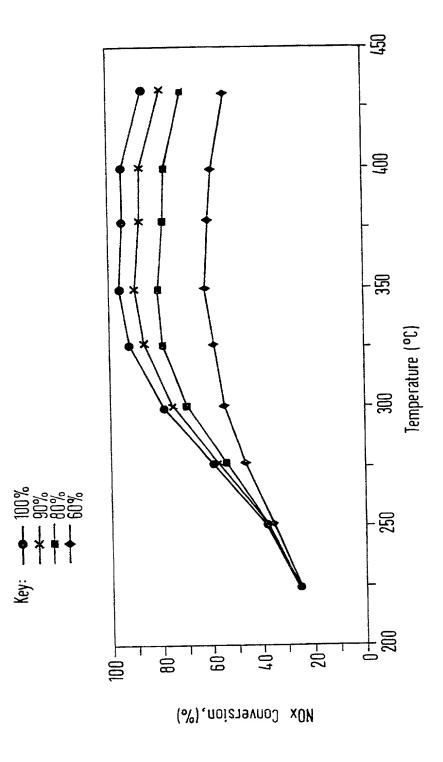
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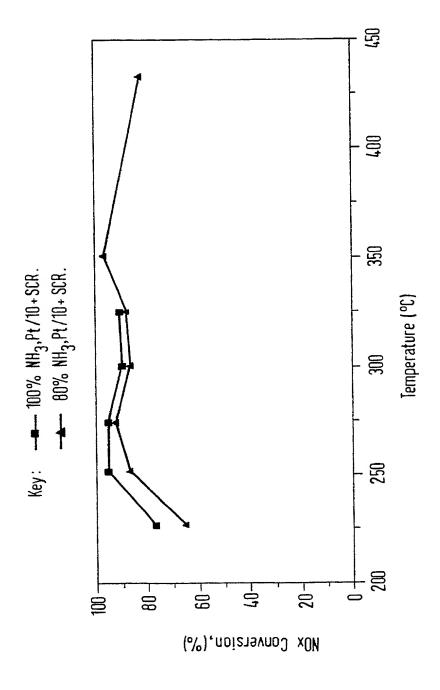
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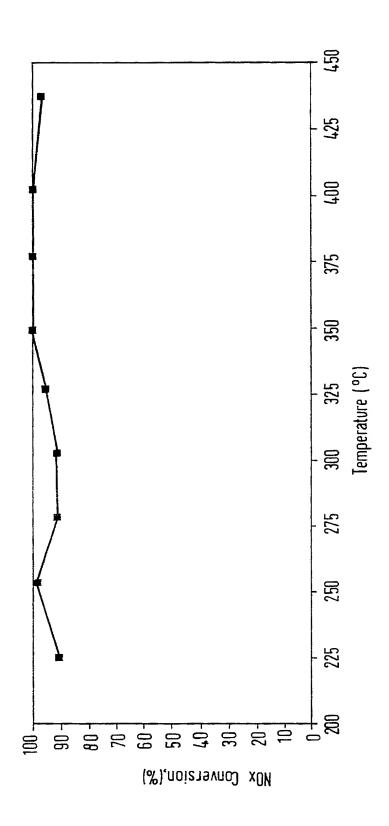
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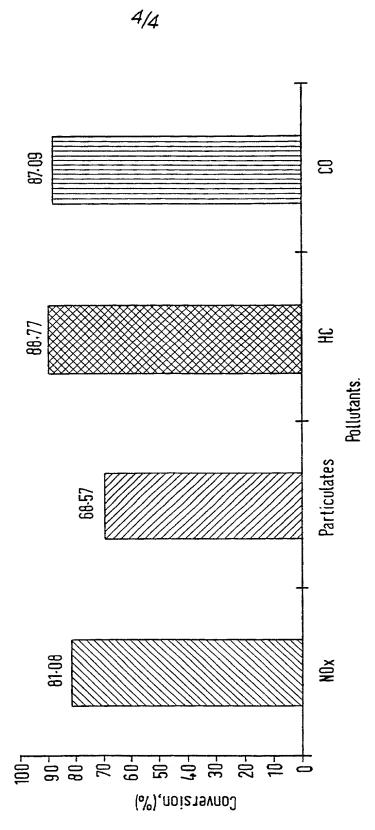




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SUBSTITUTE SHEET (RULE 26)



# Declaration and Power of Attorney For Patent Application English Language Declaration

	0 0					
As a below named inventor, I hereby declare that:						
My residence, post office add	y residence, post office address and citizenship are as stated below next to my name,					
first and joint inventor (if plura and for which a patent is sou IMPROVEMENTS IN CATAL	believe I am the original, first and sole inventor (if only one name is listed below) or an original, irst and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled <a href="MPROVEMENTS">MPROVEMENTS IN CATALYTIC REDUCTION OF NOX</a> , he specification of which is attached hereto unless the following box is checked:					
United States Application and was amended on 10 hereby state that I have revi	was filed on <u>28 January 1999</u> as  United States Application Number or PCT International Application Number <u>PCT/GB99/00292</u> and was amended on <u>10 January 2000</u> and <u>August 7, 2000</u> (if applicable).  hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.					
acknowledge the duty to dis	acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR § 1.56.					
hereby claim foreign priority benefits under 35 U.S.C. §119(a)-(d) or § 365(b) of any foreign application(s) for patent or inventor's certificate, or § 365(a) of any PCT International application which designated at least one country other than the United States, listed below and have also identified below by checking the box, any foreign application for patent or inventor's certificate, or PCT international application having a filing date before that of the application on which priority is claimed:  Prior Foreign Application(s)						
<u>9802504.2</u> Great	: Britain	6 February 1998				
(Number) (Count	ry)	(Day/Month/Year Filed)				
(Number) (Count	ry)	(Day/Month/Year Filed)				
I hereby claim the benefit unlisted below.	nder 35 U.S.C. § 119(e	e) of any United States p	rovisional application(s)			
Application Number) (Filing Date)						
(Application Number)	(Filing Date)					
I hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s), or 365(c) of any PCT International application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International application in the manner provided by the first paragraph of 35 U.S.C. § 112, acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR § 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application:						

	(Application Number)		(Filing Date)	ing Date) (Status - patented, pending,		g, abandoned)	
	—— (Application Number)		(Filing Date)	(Status - patented, pending, abandoned)		ed)	
-		cute this appli		hereby appoint the following attorney(s) and/o all business in the Patent and Trademark Office			
	Allan Ratner I Andrew L. Ney I Kenneth N. Nigon I Kevin R. Casey I Benjamin E. Leace I	Reg. No. 23,031, Reg. No. 19,717 Reg. No. 20,300 Reg. No. 31,549 Reg. No. 32,117 Reg. No. 33,412 Reg. No. 24,842	Lawrence E. Ashery Christopher R. Lewis Robert L. Andersen Joshua L. Cohen Daniel N. Calder Louis W. Beardell, Jr. Jacques L. Etkowicz	Reg. No. 34,515 Reg. No. 36,204 Reg. No. 25,771 Reg. No. 38,040 Reg. No. 27,424 Reg. No. 40,506 Reg. No. 41,738	Mark J. Marcelli Jack J. Jankovitz Jonathan H. Spadt Christopher I. Halliday Scott A. Mckeown	Reg. No. 42,690 Reg. No. 45,122 Reg. No. 42,621 Reg. No. 42,866	
The state of		Suite 301, On	Paul F. Prestia e Westlakes, Berwyr ul F. Prestia at (610)		Valley Forge, PA_1	9482-0980	
	statements made were made with the fine or imprisonme willful false stateme	on information e knowledge t ent, or both, ur ents may jeopa	atements made her and belief are belief that willful false stander Section 1001 of ardize the validity of hame, family hame Ander	eved to be true; tements and th f Title 18 of the the application o	and further that the like so made are United States Cod	nese statements e punishable by le and that such	
1	Inventor's signature	Anders	Andreasson	SIS ANDREASSON	Date <u>/ 3 / / 2</u>	-2000	
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		0 1	(given name, family nam	e) <u>Guy Richard Ch</u>	HANDLER Date	-// - 00	
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	Additional invent	tors are being nan	ned on separately numbe	red sheets attached	hereto.		

2
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Seventh inventor's signature Date
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